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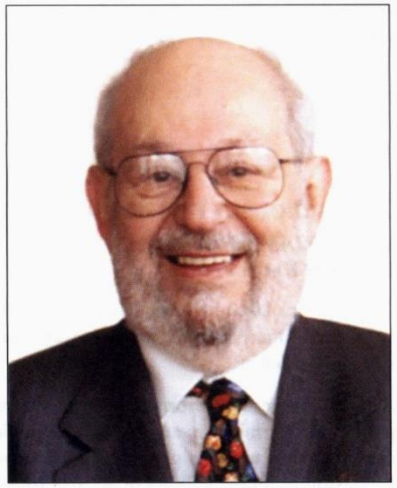

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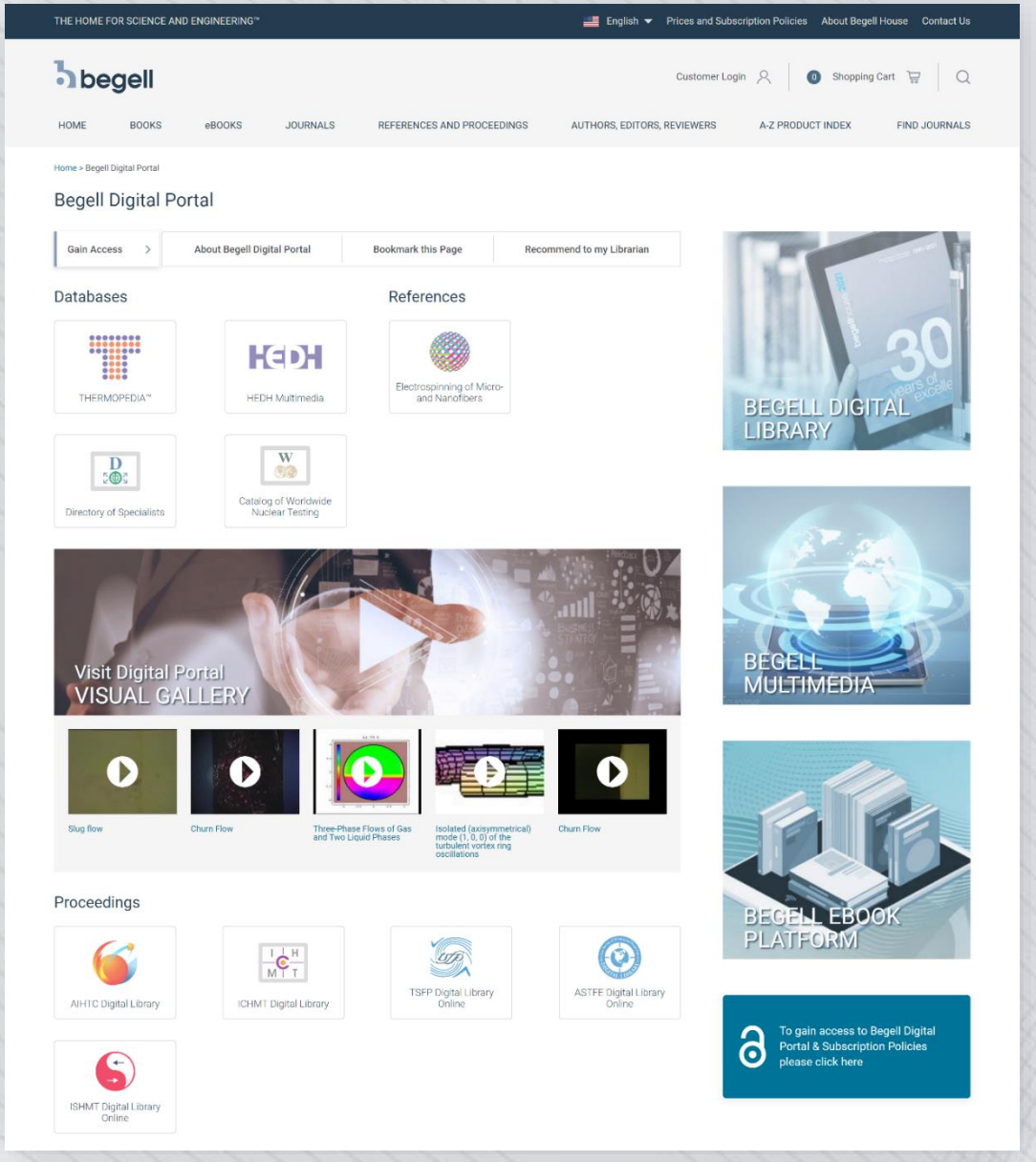

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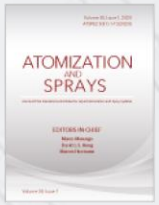

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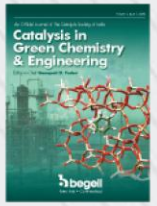

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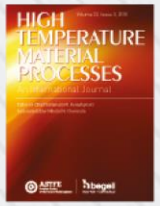

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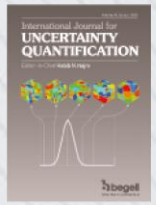

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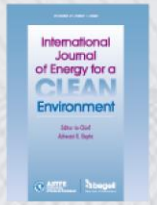

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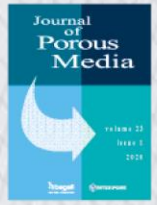

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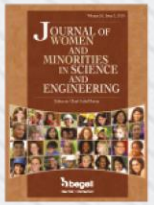

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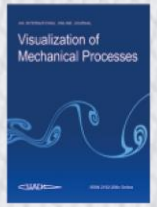

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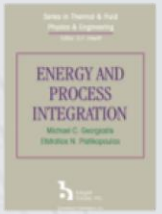

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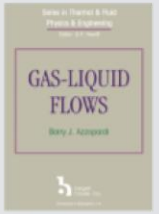

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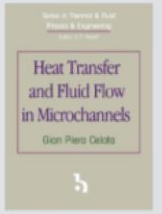

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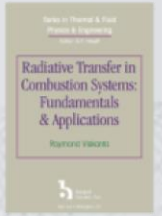

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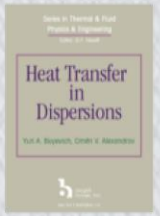

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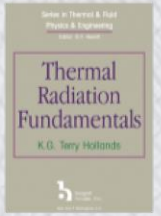

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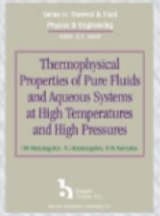

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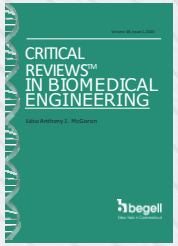

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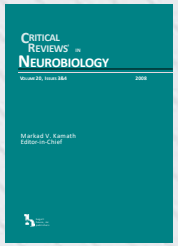

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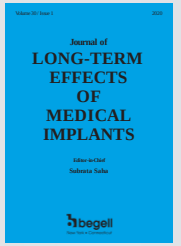

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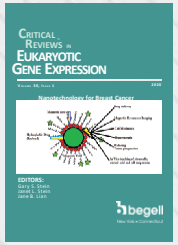

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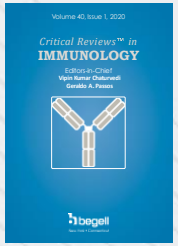

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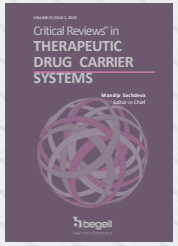

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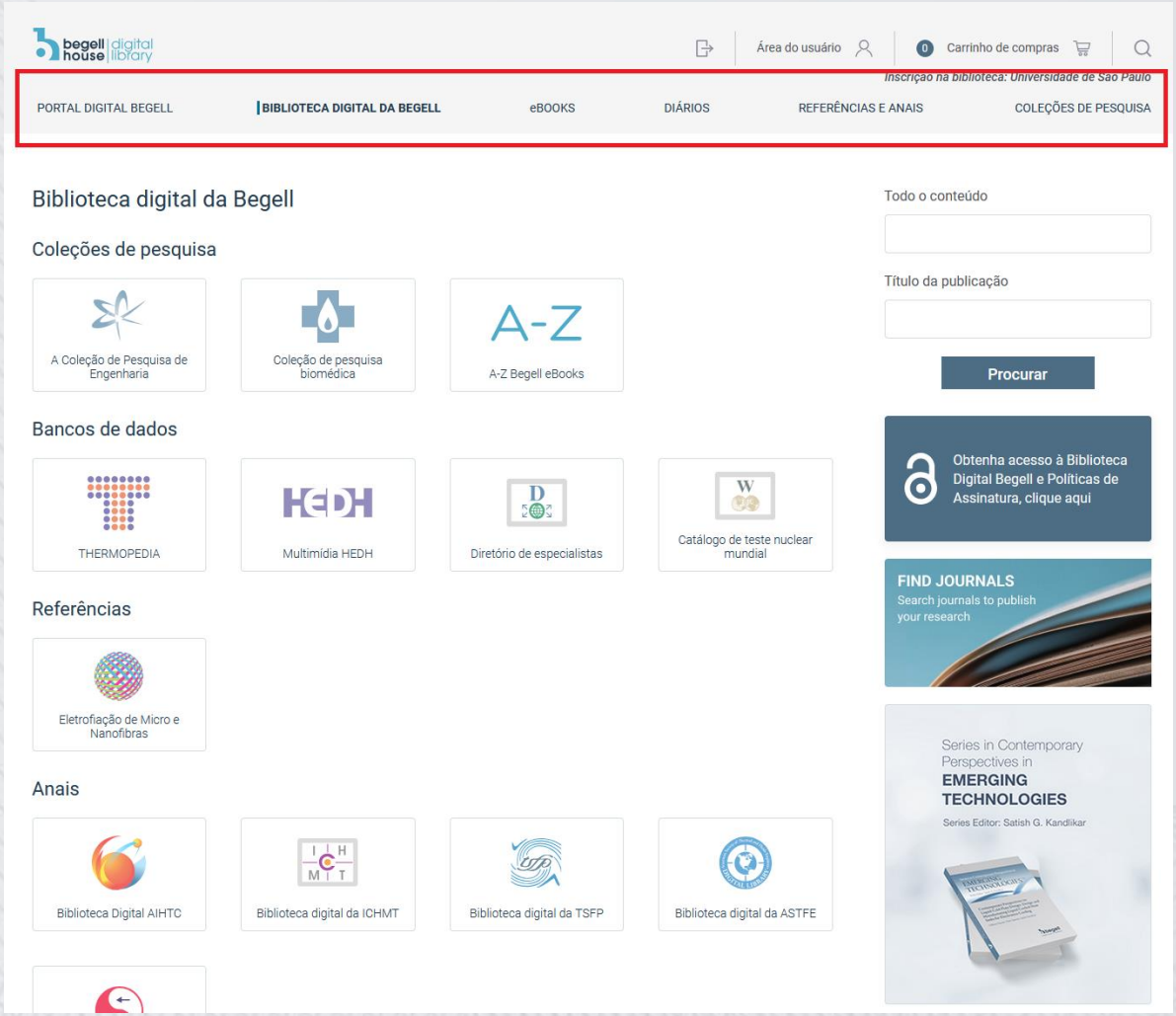

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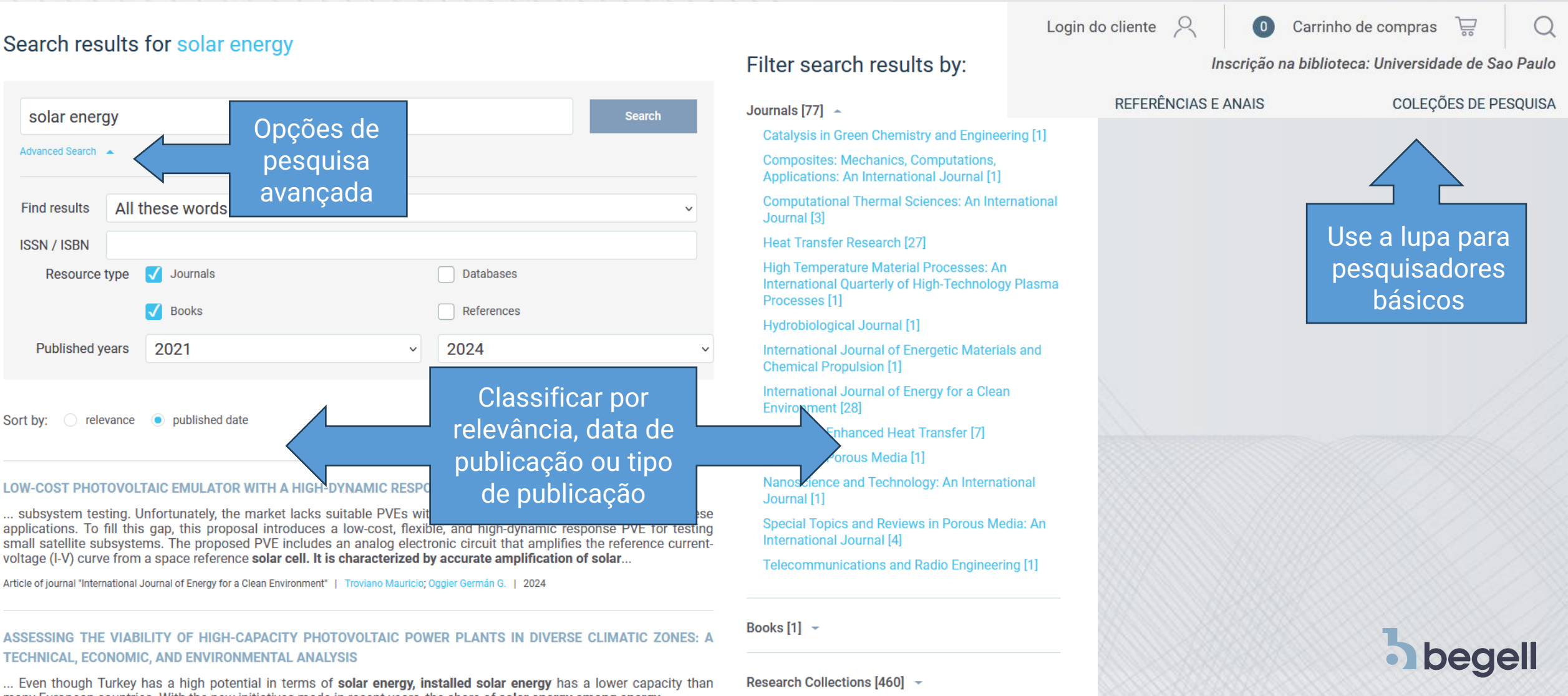

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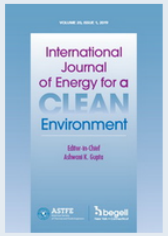

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LOW-COST PHOTOVOLTAIC EMULATOR WITH A HIGH-DYNAMIC RESPONSE FOR SMALL SATELLITE APPLICATIONS

Volume 25, Edição 6, 2024, pp. 1-12

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RESUMO

In recent years, growing interest from academic institutions and emerging countries in small satellite missions has led to a need for photovoltaic emulators (PVEs) during subsystem testing. Unfortunately, the market lacks suitable PVEs with adequate power and characteristics for these applications. To fill this gap, this proposal introduces a low-cost, flexible, an tellite subsystems. The proposed PVE includes an analog electronic ci V) curve from a space reference solar cell. It is characterized by ac ous conditions, achieving a maximum output power of 124 W. This ca application scenarios with rapidly changing climatic conditions. The emulator's remarkable flexibility is demonstrated through the use of various solar cell technologies for space applications as references. Experimental results effectively confirm the practical feasibility of the proposed PVE.

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Palavras-chave: photovoltaic emulator, space solar cells, small satellite development, Space Solar Array Simulator

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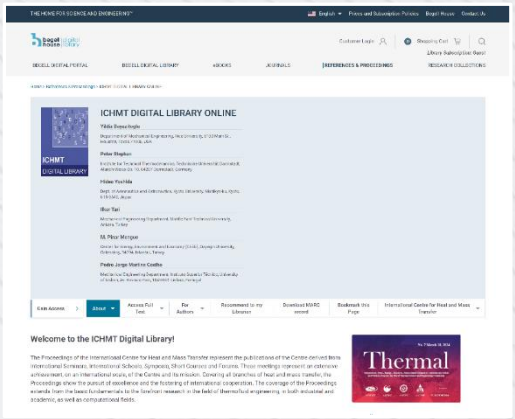

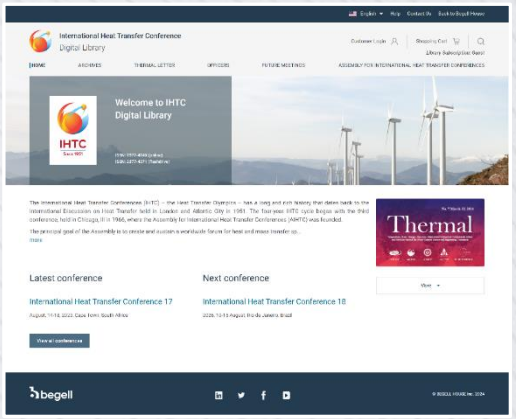

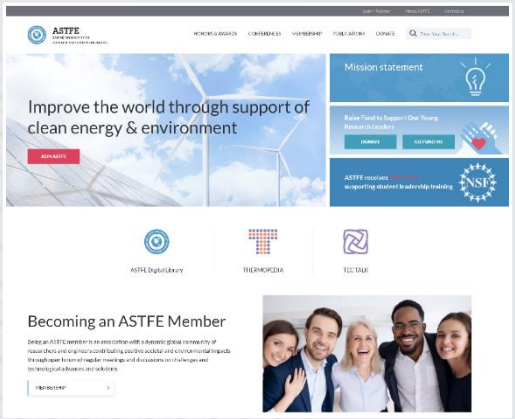

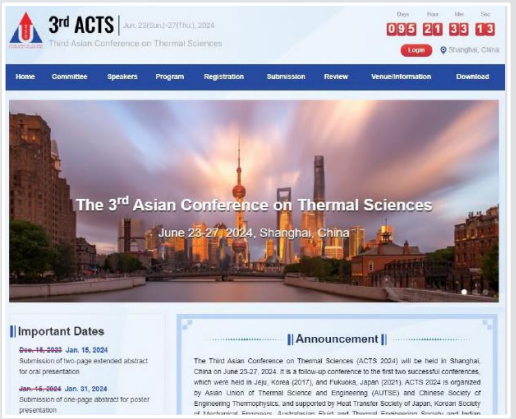

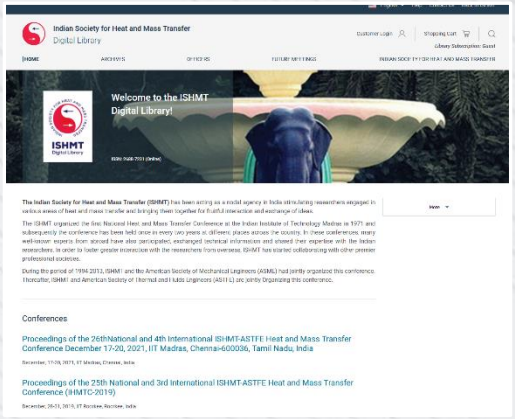

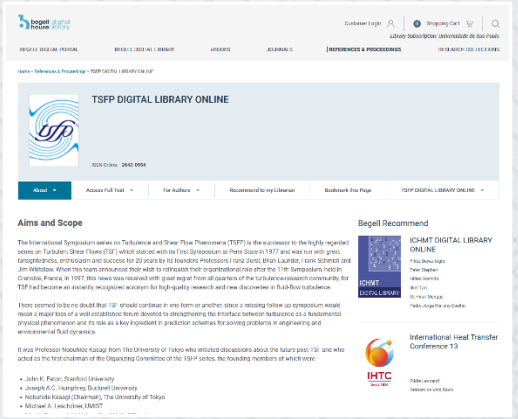

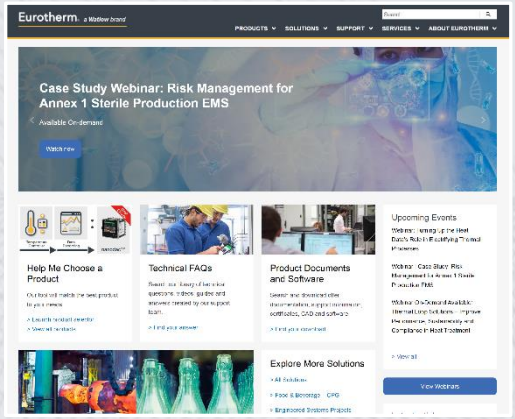

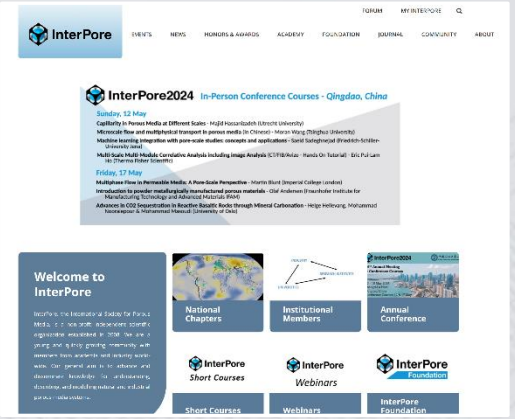

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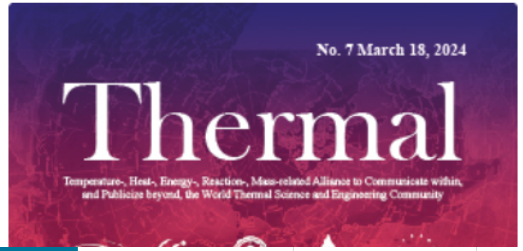

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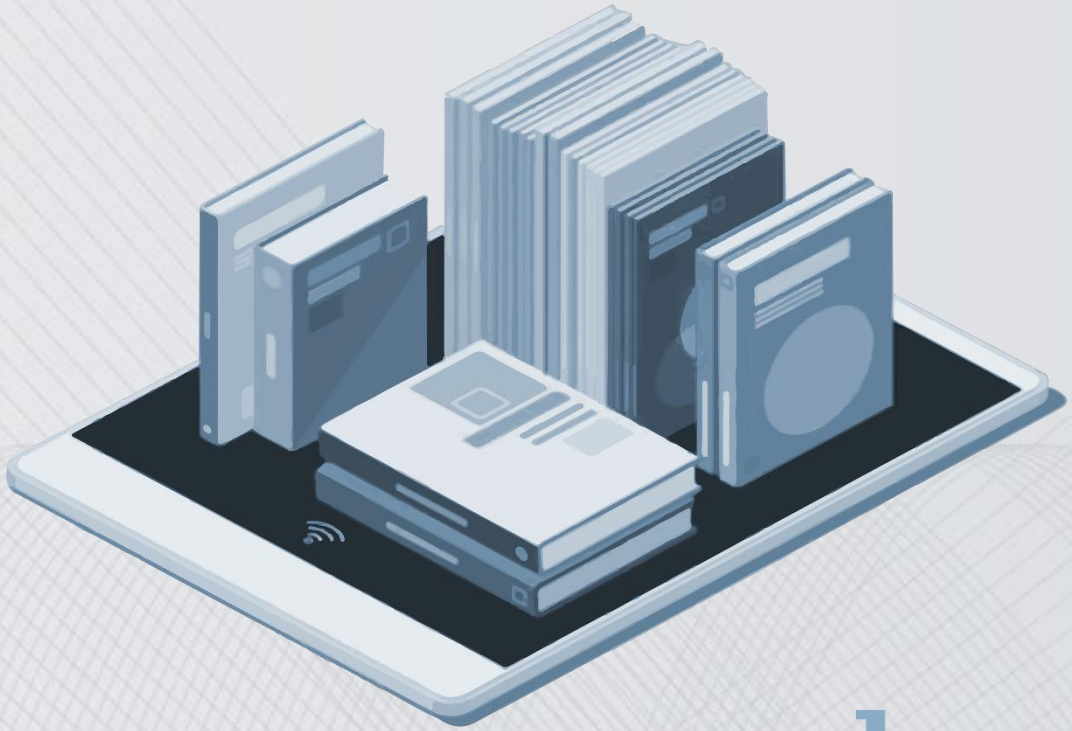

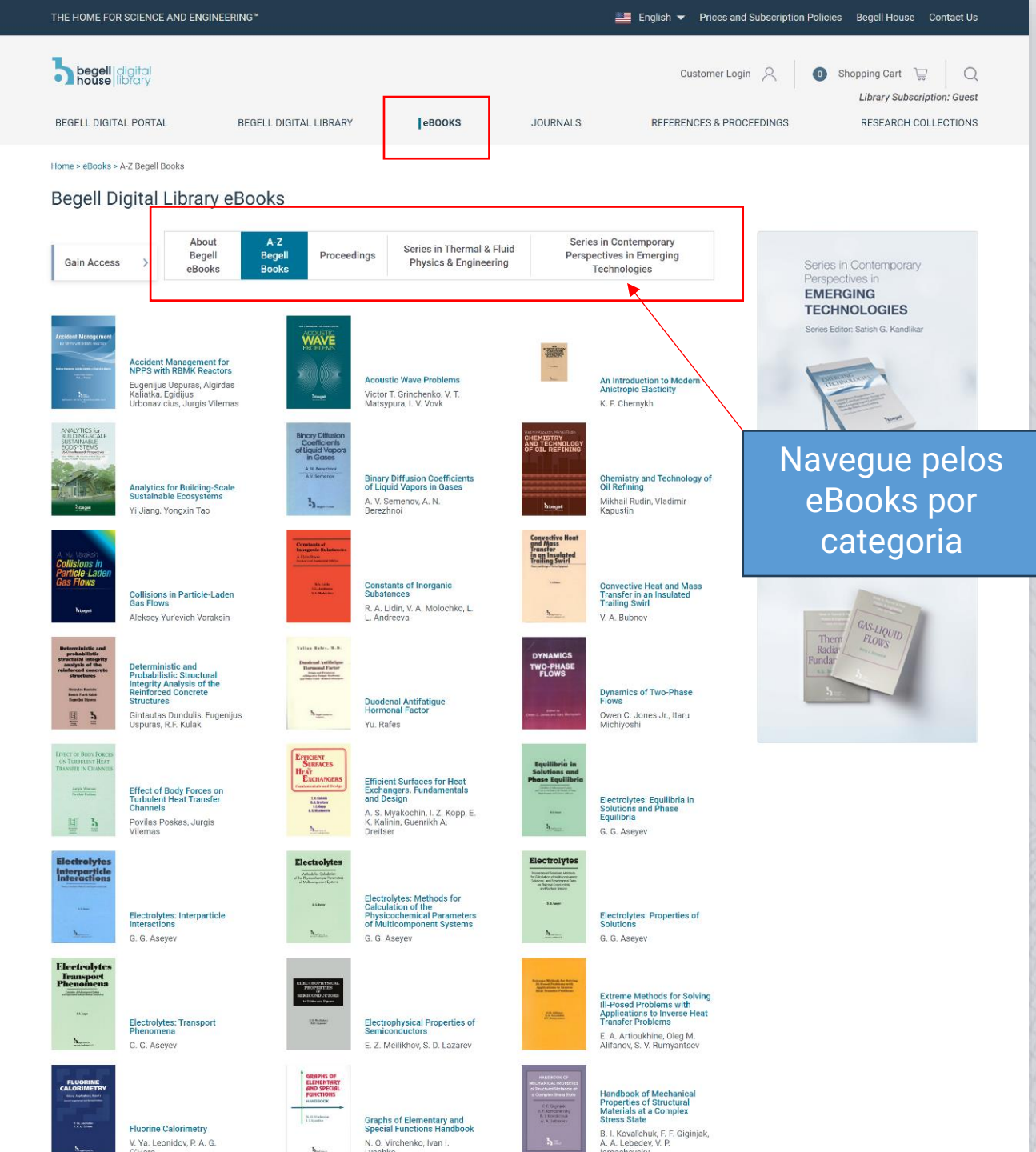

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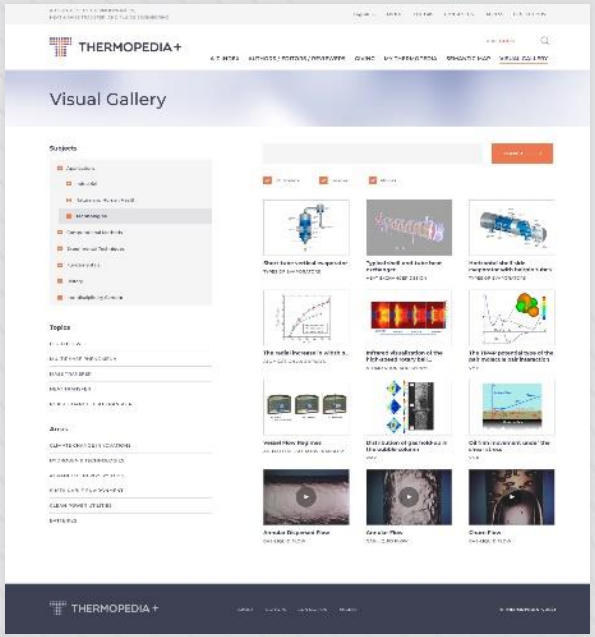

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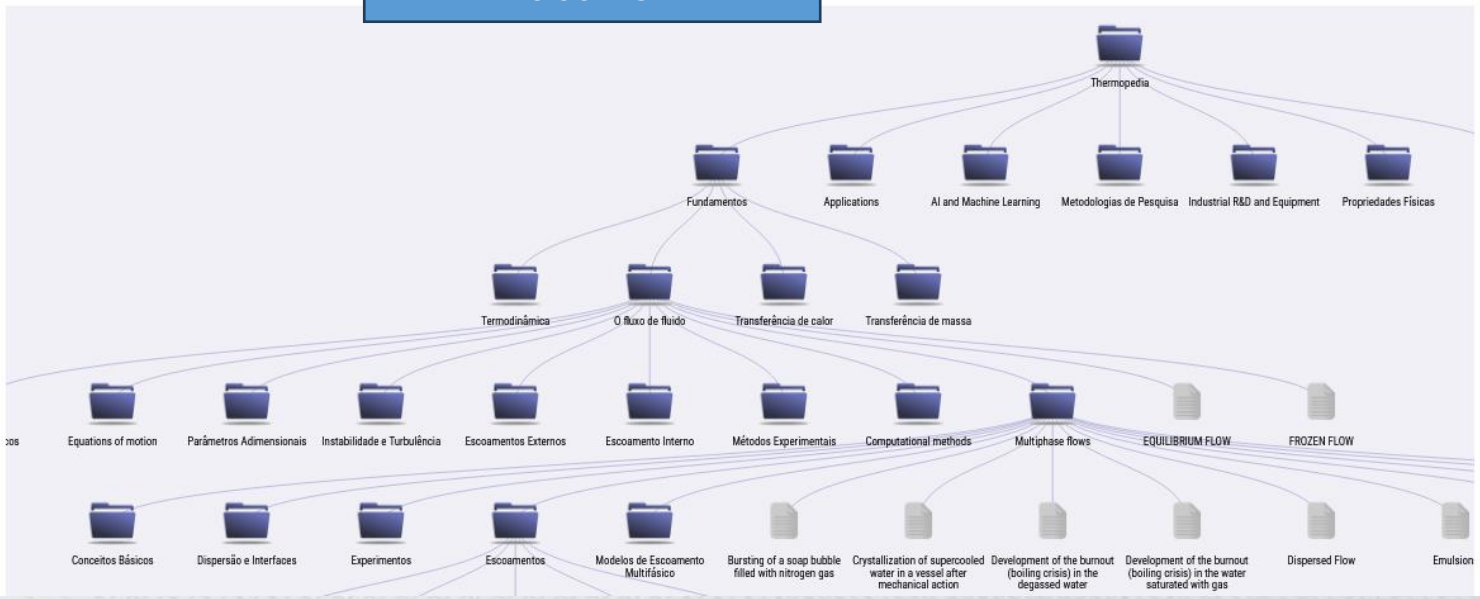

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Hewitt, Geoffrey F. | DOI: 10.1615/AtoZ.g.gas-liquid_flow

Article added: 7 September 2010 | Article last modified: 25 May 2011

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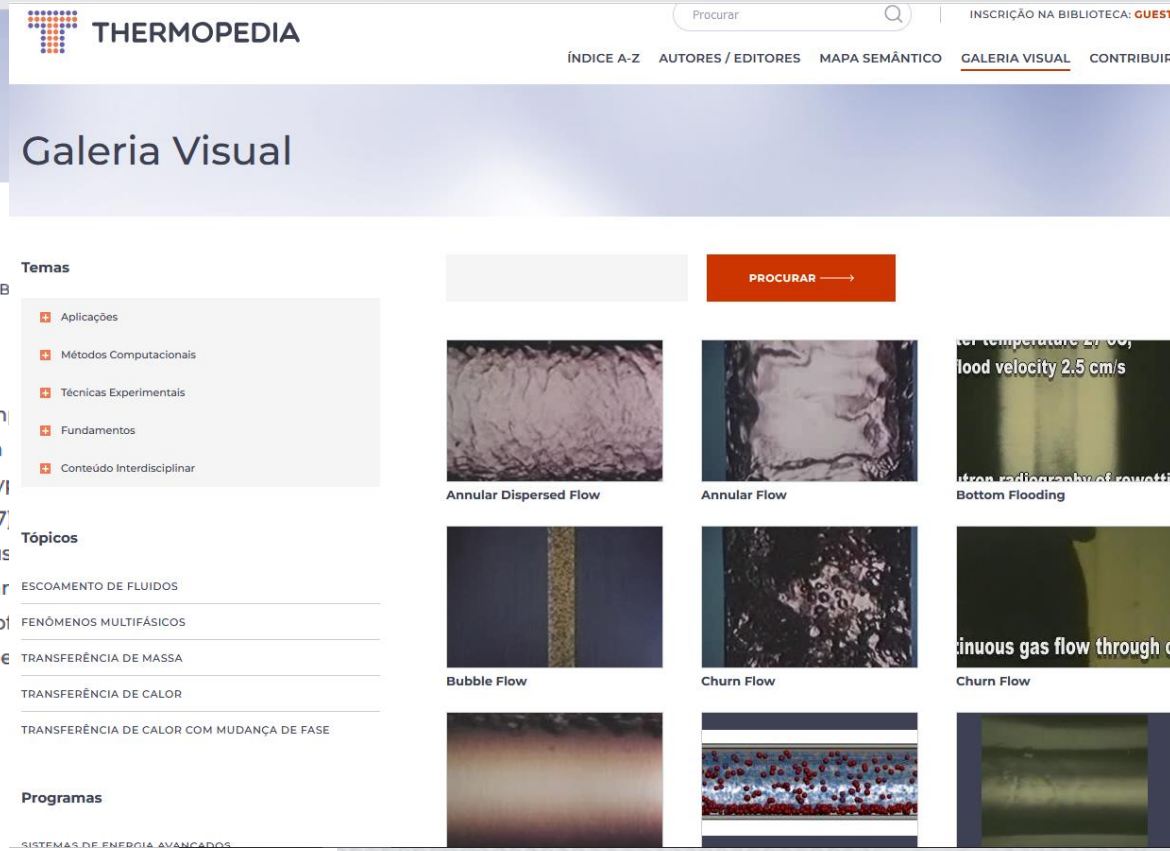
Of the four type of Two-Phase Flow (Gas-Liquid, Gas-Solid, Liquid-Liquid and Liquid-Solid), gas-liquid flows are the most com
characteristics of a deformable interface and the compressibility of one of the phases. For given flows of the two phases in a
interfacial distribution can take any of an infinite number of possible forms. However, these forms can be classified into ty
commonly called *flow regimes* or *flow patterns*. Detailed discussions of these patterns are given by Hewitt (1982), Whalley (1987
The regimes encountered in vertical flows are illustrated in Figure 1. They include Bubble Flow, where the liquid is continuous
bubbles within the liquid; Slug or Plug Flow where the bubbles have coalesced to make larger bubbles which approach the diar
where the slug flow bubbles have broken down to give oscillating churn regime; Annular Flow where the liquid flows on the wall o
liquid entrained in the core) and the gas flows in the centre; and Wispy Annular Flow where, as the liquid flow rate is increased, the
gas core increases, leading to the formation of large lumps or streaks (wisps) of liquid.

Bubble Flow ( )Slug or Plug Flow ( )Churn Flow ( )Annular Flow ( )Wispy Annular Flow ( )

Figure 1. Flow patterns in vertical flow (All Flows).

Flow regimes in horizontal flow are illustrated in Figure 2. Here, as gravity acts normally to flow direction, separation of the flow occurs. The respec

Hyperlinks to references and related articles (orange)



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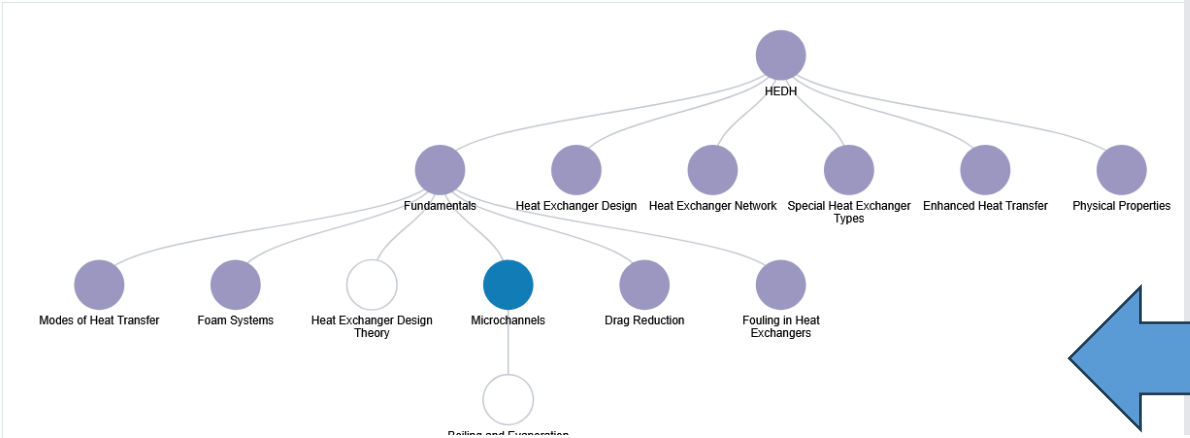

Clicar nos círculos expande os subtópicos e termos relacionados

Click here to open **Visual Navigation**

Number of views: 12468

Fundamentals > Microchannels

Boiling and Evaporation

DOI 10.1615/hedhme.a.000228

Sujoy Kumar Saha and Gian Piero Celata

A. Introduction

Microcooling elements in micro-thermal-mechanical systems (MTMS) are a modern high-end technology. Microchannel heat sinks are extensively used in high-heat flux systems, e.g., microelectronic, optical and microfluidic devices, high-performance supercomputers, power and laser devices, very-high temperature gas-cooled reactors and liquid metal fast reactors, radiator panels of spacecraft, thermal control of satellites, etc. In pharmaceutical and chemical industries, by integrating heat exchangers, mixers, and reactors as a significant decrease in the system size. Heat exchangers based on microscale channels are used in automotive fuel cells where the heat dissipation system should be compact and contain a minimum number of components. The heat dissipation rate is extremely high in cooling are very important in such devices due to possible higher heat transfer coefficients and much lower temperature gradients along the heat exchanger. In addition, two-phase microchannel heat sinks are one of the strongest candidates for heat removal devices in h area-to-volume ratio, compact dimensions, and low flow rate requirements. Flow boiling in microchannels has drawn considerable attention from researchers worldwide. Microchannels are used in MEMS and high-end microprocessor cooling applications. Microchannels pressures (up to 600 bar) and temperatures (1,000 °C). There is a scale effect that becomes evident when the hydraulic diameter is less than the capillary length, i.e., $[(\sigma/\boldsymbol{g})(\rho_l - \rho_v)]^{0.5}$.

In microchannels, the hydraulic diameter of the channels is smaller than the capillary length. Identifying the threshold, or the transition band, beyond which a two-phase flow may be considered "micro" is an open issue. The channel classification has been giv should be used as a mere guide indicating the size range, rather than rigid demarcations based on specific criteria. Relevant literature in this direction would be Kawaji and Chung (2003). The confinement number ($\mathbf{Co}$), as the distinguishing parameter, gives only a rough

$$\mathrm{Co} = \frac{1}{D}\sqrt{\frac{\sigma}{(\rho_l - \rho_v)\, g}} \qquad (1)$$

Suo and Griffith (1964) set $\mathbf{Co}_{\boldsymbol{H}}$ = 3.3, and Kew and Cornwell (1997) sugg .5, whereas that suggested by Brauner and Moalem Maron (1992) is 0.16.

1e-7 m
1e-4 mm
3.281e-7 ft
3.937e-6 in

Two sets of classifications based on the hydraulic diameter were given b et al. (2000a) and Kandlikar et al. (2001). According to Mehendale et al. (2000a), a microchannel is 1-100 μm, mesochannel 100 μm-1 mm, compact passages 1-6 mm, and conventional channels >6 mm. According to Kandlikar et al. (2001), a molecular nanochannel is <0.1 μm, transitional nanochannel 0.1–1 μm, transitional microchannel 1–10 μm, microchannel 10–200 μm, minichannels 200 μm-3 mm, and conventional channels >3 mm.

A more general definition would have to address situations where classical theory is no longer fully applicable, that is, it no longer correctly predicts the mechanical and thermal process in terms of friction and heat transfer. The definition also depends on the fluid and the working conditions.

Feng and Serizawa (2000) define a microchannel as being one in which theLaplace constant is larger than the diameter of the channel. They categorized their observations of flow regimes as follows: bubble flow, elongated bubble (or slug) flow, annular flow, liquid ring flow, liquid lump flow, and mist flow.

Another criterion is when the bubble departure diameter is larger than the channel diameter, such that bubble growth is confined by the size of the channel cross section (there are many bubbles in a macrochannel). Hence, the threshold to confined bubble flow could be taken as the microscale threshold. The bubble departure diameter in nucleate pool boiling $d_{\mathrm{bub},\boldsymbol{P}}$ is given (Fritz, 1935) by

$$d_{\mathrm{bub},F} = 0.0208\,\beta\left[\frac{\sigma}{g\,(\rho_L - \rho_G)}\right]^{1/2}$$

where the contact angle β is in degrees and the effect of cross flow on bubble departure is ignored. For application to a wider range of pressures,

Adicionar aos gerenciadores de citações

Todos os artigos incluem:

- Hiperlinks para referências, figuras e artigos relacionados
- Conversões de unidades no texto

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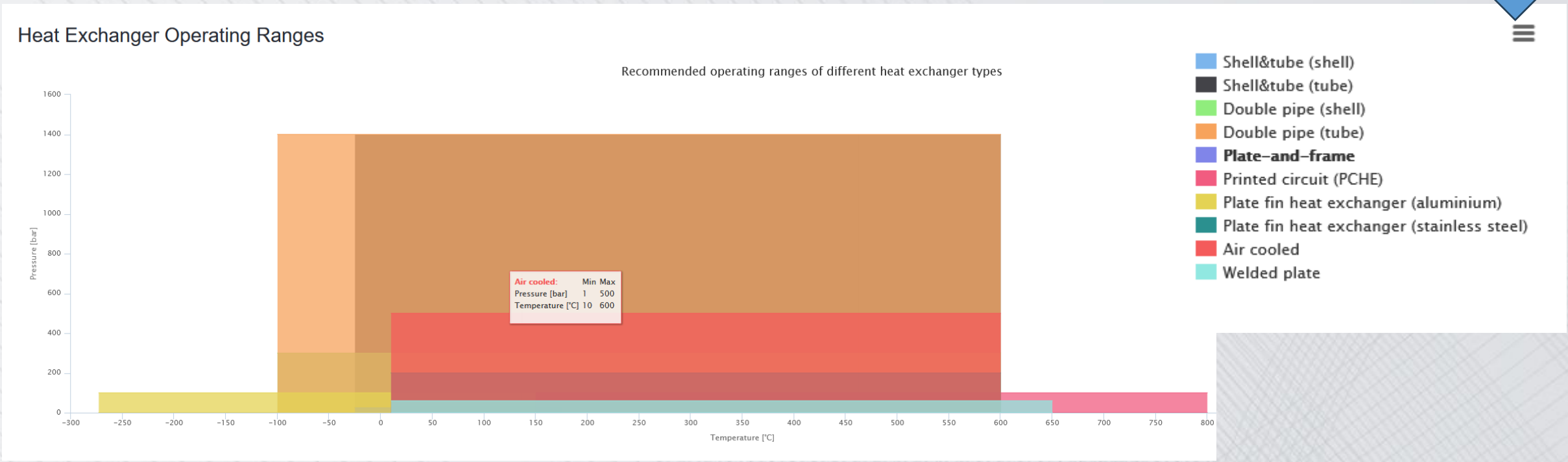
Widget de Faixas de Operação do Trocador de Calor

Passe o mouse sobre cada bloco para mais detalhes

Clique nos blocos ou use este menu lateral para selecionar ou desmarcar o tipo de trocador de calor

Imprimir/exportar a imagem para apresentações



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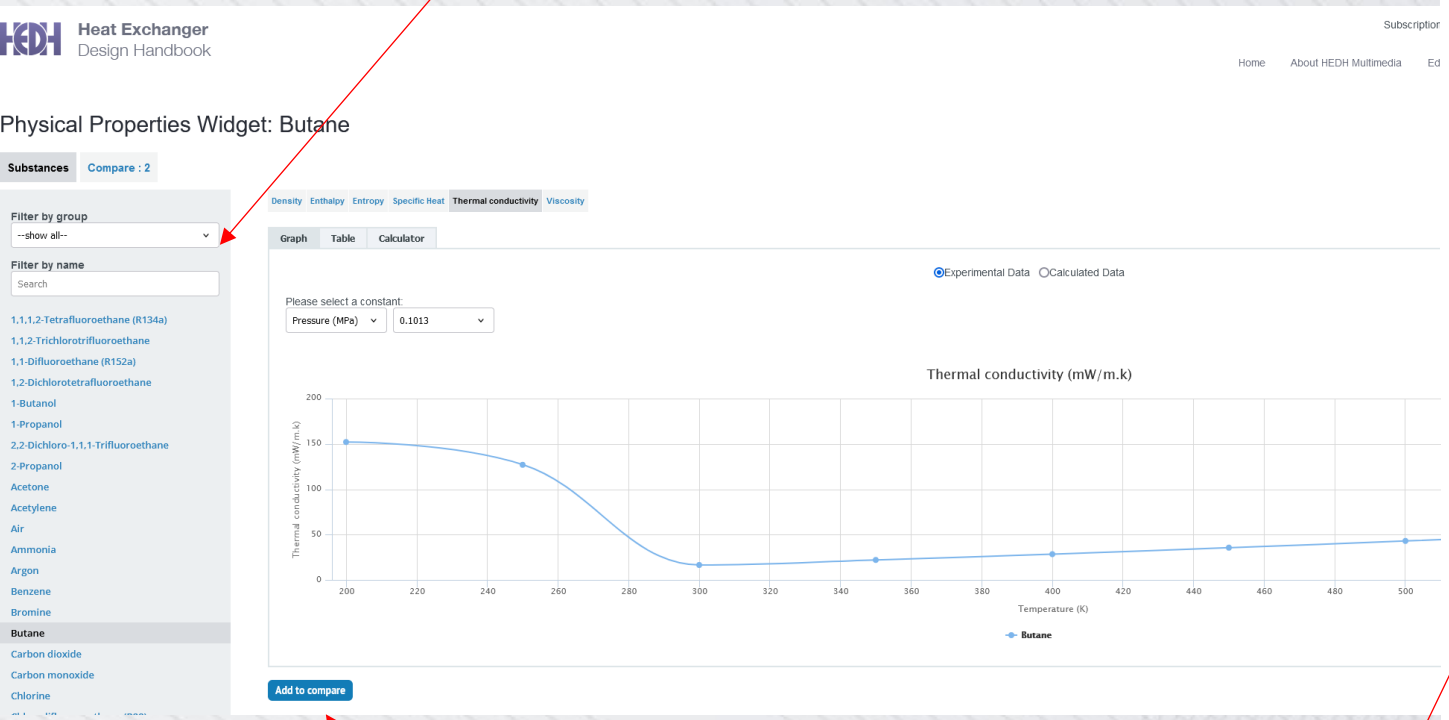
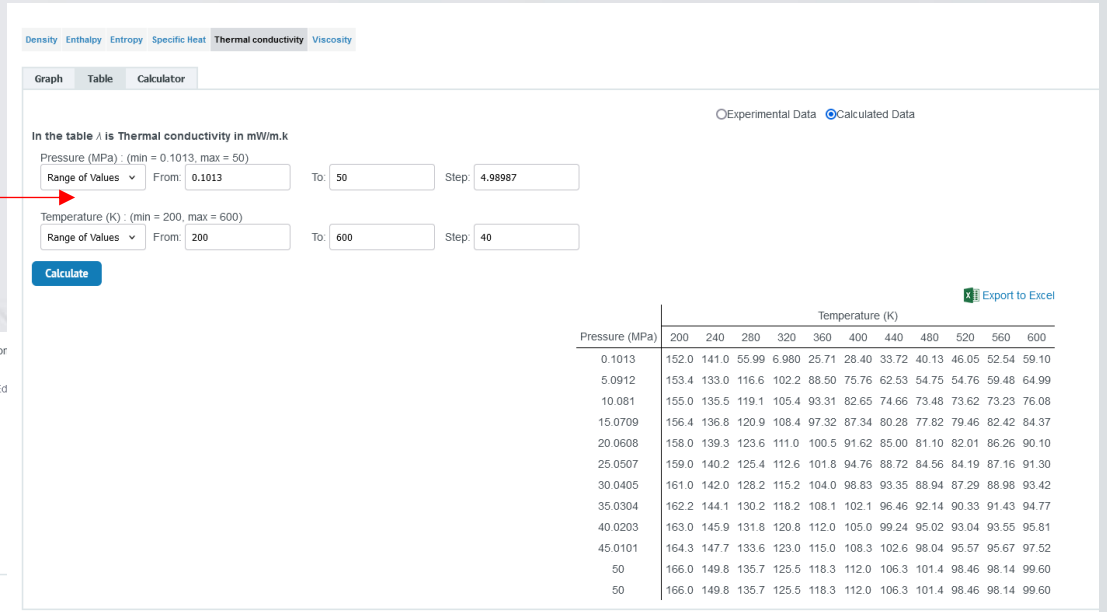
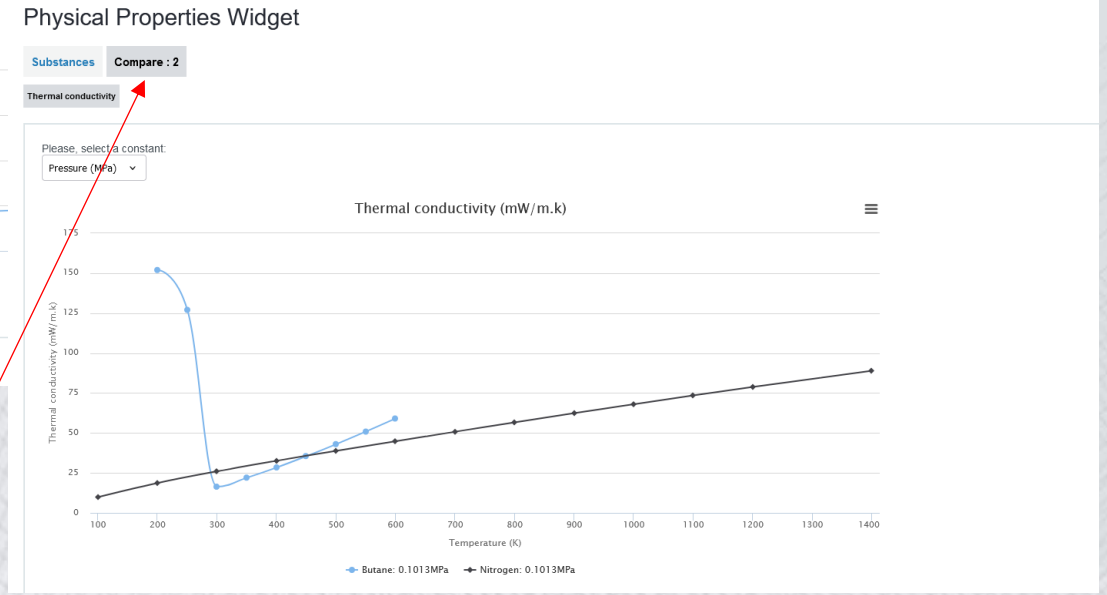
Widget Propriedades físicas

Escolha substâncias da lista para visualizar suas propriedades físicas como um gráfico ou tabela. OU selecione "calculadora" para inserir e mapear seus próprios dados





Pressure (MPa)	Temperature (K) 200	240	280	320	360	400	440	480	520	560	600
0.1013	152.0	141.0	55.99	6.980	25.71	28.40	33.72	40.13	46.05	52.54	59.10
5.0912	153.4	133.0	116.6	102.2	88.50	75.76	62.53	54.75	54.76	59.48	64.99
10.081	155.0	135.5	119.1	105.4	93.31	82.65	74.66	73.48	73.62	73.23	76.08
15.0709	156.4	136.8	120.9	108.4	97.32	87.34	80.28	77.82	79.46	82.42	84.37
20.0608	158.0	139.3	123.6	111.0	100.5	91.62	85.00	81.10	82.01	86.26	90.10
25.0507	159.0	140.2	125.4	112.6	101.8	94.76	88.72	84.56	84.19	87.16	91.30
30.0405	161.0	142.0	128.2	115.2	104.0	98.83	93.35	88.94	87.29	88.98	93.42
35.0304	162.2	144.1	130.2	118.2	108.1	102.1	96.46	92.14	90.33	91.43	94.77
40.0203	163.0	145.9	131.8	120.8	112.0	105.0	99.24	95.02	93.04	93.55	95.81
45.0101	164.3	147.7	133.6	123.0	115.0	108.3	102.6	98.04	95.57	95.67	97.52
50	166.0	149.8	135.7	125.5	118.3	112.0	106.3	101.4	98.46	98.14	99.60
50	166.0	149.8	135.7	125.5	118.3	112.0	106.3	101.4	98.46	98.14	99.60



Para mapear/comparar várias substâncias:

- Selecione cada substância e clique em "Adicionar para comparar"
- Em seguida, clique em "Comparar: 2" no canto superior esquerdo

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Assistente de seleção de tipo de condensador

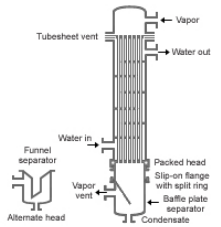
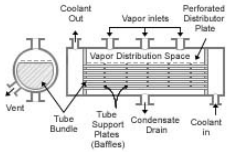
Condenser Type Selection Wizard

Wizard by F. Coletti, information by A.C. Muller, D. Butterworth, H.R. Jacobs

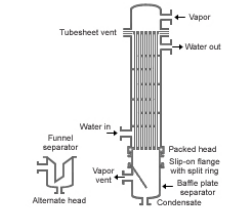
Condenser design involves evaluation of the specified process conditions, together with other potential physical, thermal, and economic limits in order to select potential types of cond ited to determine the best economic choice. This design must meet certain basic requirements: (1) it must be operable over a range of conditions including design point... read more

Step 1: Select type of condensation	Partial	Total	
Step 2: Select operating pressure	Very low (P<1 bar)	Intermediate (1<P<25 bar)	High (P>25 bar)
Step 3: Select vapor characteristics	Non corrosive	Corrosive	Very corrosive
Step 4: Select operating temperature	Low (T<400°C)	High (T>400°C)	
Step 5: Select fouling characteristics	Moderate	Severe coolant	Severe vapor
Step 6: Can the condensate freeze?	No	Yes	
Step 7: Is the vapor single or multicomponent?	Single component	Multiple component	
Step 8: Is the gas noncondensable?	No	Yes	
Step 9: Tube-side pressure drop	Low	High	
Step 10: What phase is the coolant in?	Liquid	Gas	Boiling
Step 11: Can the two fluids be mixed?	No	Yes	

Reset

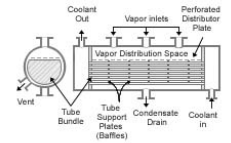
	Preferred Configuration	Optional Configuration
Fluid allocation:	Tube-side condensation	Shell-side condensation
Orientation:	Vertical	Horizontal
Configuration:	Downflow	Cross "X"
Acceptability:	Good	Fair
Predictability:	<50%	<50%
Acceptability pressure drops:	Good	Good
Predictability pressure drops:	>50%	<50%
Advantages:	Good control of venting. Handles dirty or polymerizing vapors.	Can handle freezing condensate. Good control of venting. Can use finned or enhanced tubes.
Disadvantages:	Poor for pressure below 25 mmHg absolute. Tubesheet vents required.	-
Notes:	-	-
		
Relevant section	read more...	read more...

Preferred Configuration



Fluid allocation: Tube-side condensation
Orientation: Vertical
Configuration: Downflow
show details

Optional Configuration



Fluid allocation: Shell-side condensation
Orientation: Horizontal
Configuration: Cross "X"
show details

<< Compare options

Responda à lista dinâmica de perguntas para identificar o tipo de equipamento correto para o seu projeto

Clique em "Leia mais" para ver o relevante Artigo em texto completo

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Assistente de configuração de tipo TEMA

TEMA Type Configuration Wizard

DID YOU KNOW?

The TEMA type configuration wizard allows to generate and visualize the possible configurations of shell-and-tube heat exchangers according to the Tubular Exchanger Manufacturers Association standards.

Construa seu próprio trocador de calor selecionando o equipamento

Passe o mouse sobre cada opção para ver detalhes, pontos positivos e negativos

Front Head Types

A — Channel and removable cover

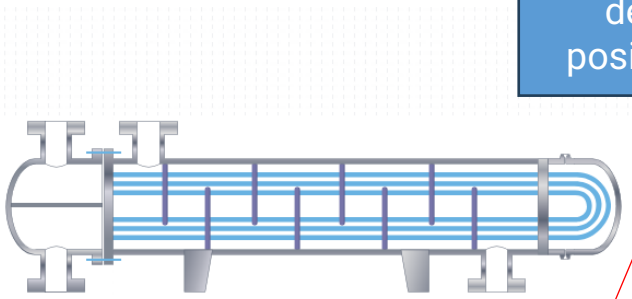
B — gral cover)

C — Channel integral with tubesheet and removable cover

D — Special high pressure closure

N — Channel integral with tubesheet and removable cover

BEU with Segmental Baffles



Shell Types

E — One pass shell

F — Two pass shell with longitudinal baffle

G — Split flow

H — Double split flow

I

K — Kettle type reboiler

X — Cross flow

Baffle Types

L — Single segmental

M — Double segmental

Two shells side passes separated by a longitudinal baffle.
Advantages: provides pure countercurrent flow in a two tube-side pass unit, allows for close approach temperature.
Disadvantages: possible leakages across the longitudinal baffle.

Rear Head Types

L — Fixed tubesheet like `A` stationary head

M — Fixed tubesheet like `B` stationary head

N — Fixed tubesheet like `C` stationary head

P — Outside packed floating head

S — Floating head with backing device

T — Pull through floating head

U — U-tube bundle

W — Externaly sealed floating tubesheet

Save as PDF

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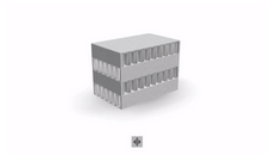
Galeria Visual HEDH

Visual Gallery



Compact Heat Exchangers
Illustration of plate fins stacked for a cross-flow heat exchanger configuration.
INTERACTIVE VERSION

Double Pipe
Simple double pipe arrangement.
INTERACTIVE VERSION

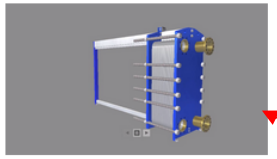
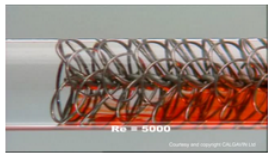


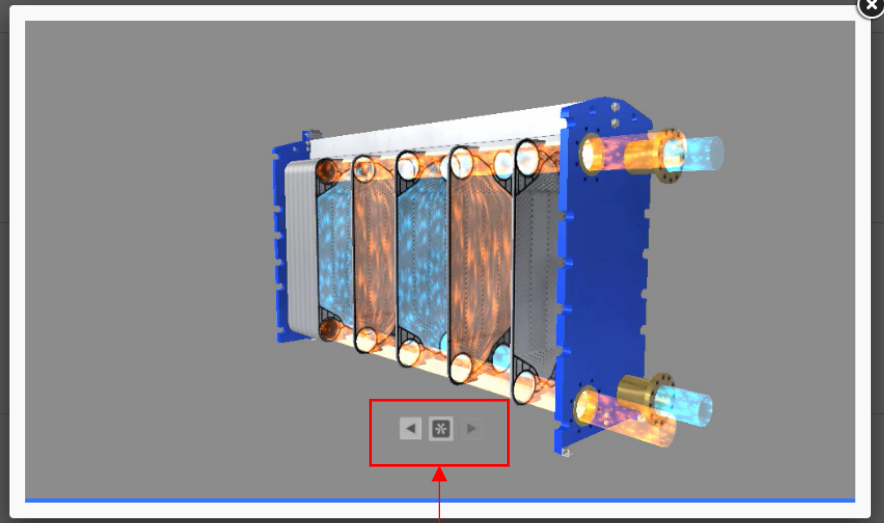
Plate and frame heat exchangers
The plates are clamped together in a frame between a fixed head plate (or head)...
INTERACTIVE VERSION

Shell-and-Tube
Typical shell-and-tube heat exchanger.
INTERACTIVE VERSION



Tube Inserts
Effects of tube inserts. Curtesy and copyright CalGavin Ltd

- Clique no título para ver o artigo em texto completo relacionado
- Clique em "Versão interativa" para abrir o modelo 3D
- Clique na miniatura para assistir ao vídeo



Use essas setas para desmontar o modelo

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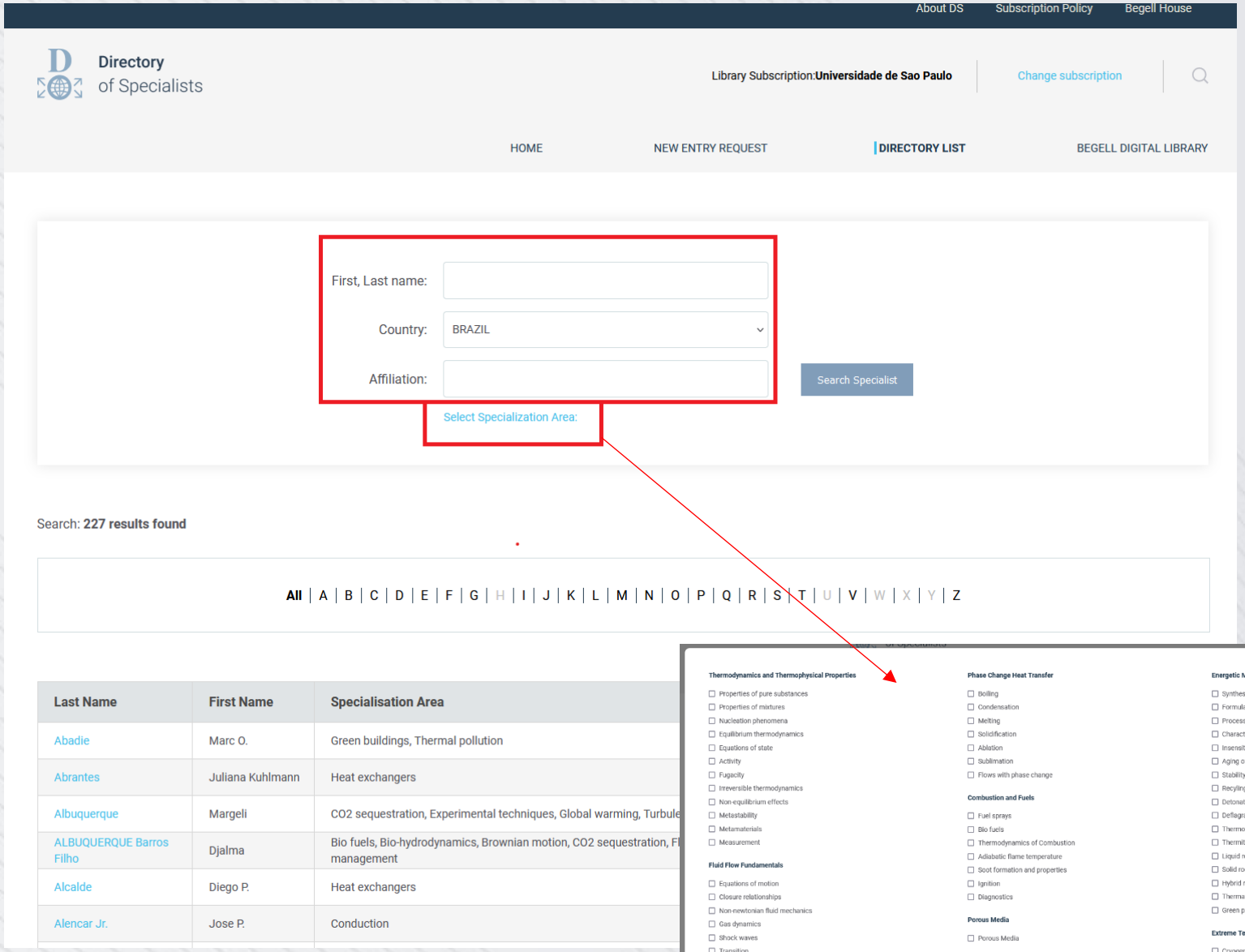

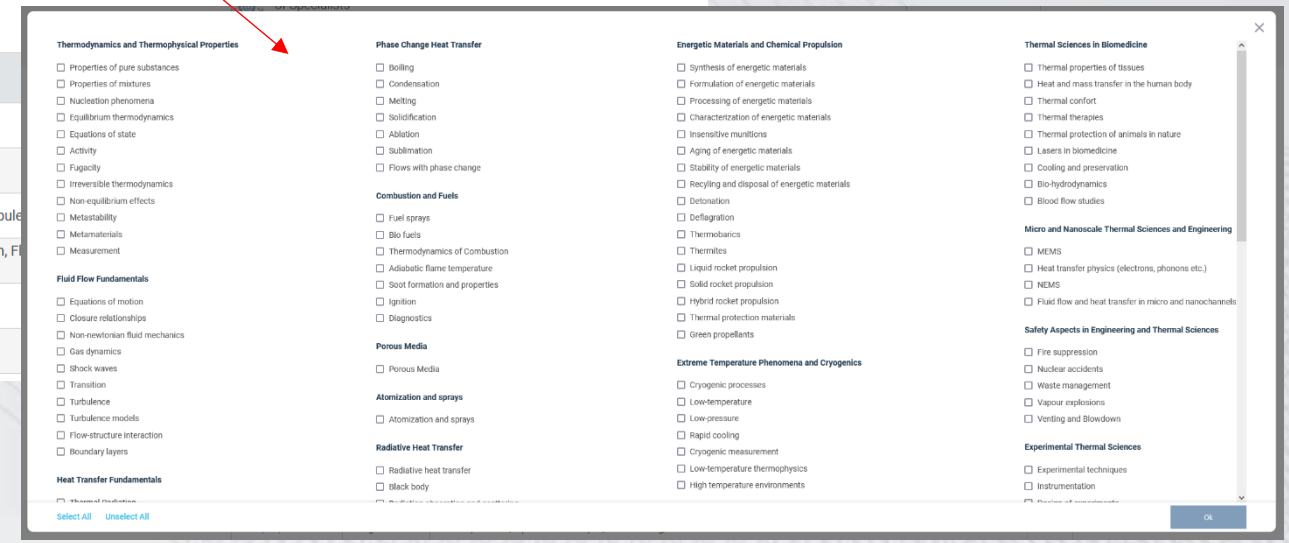

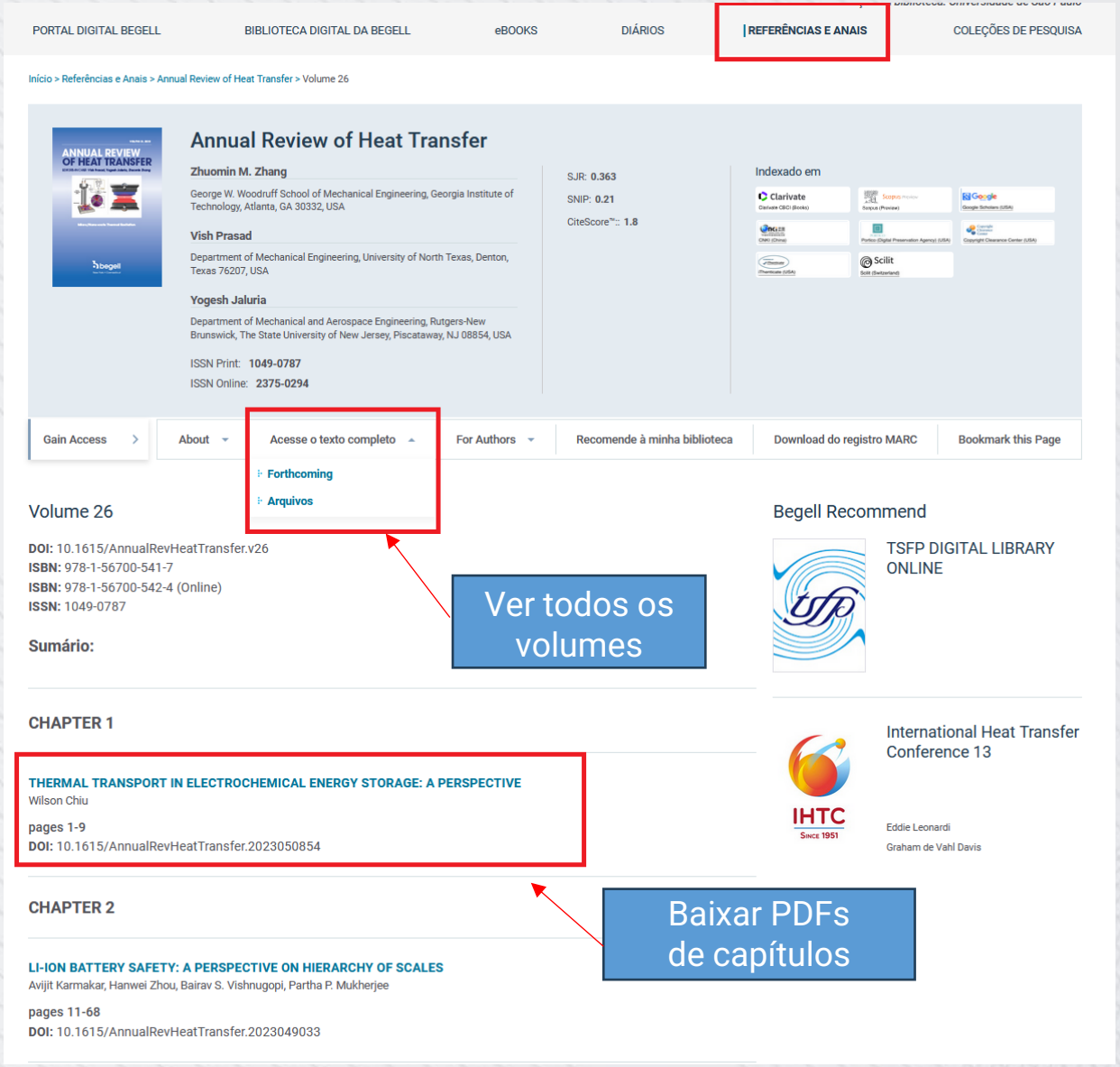

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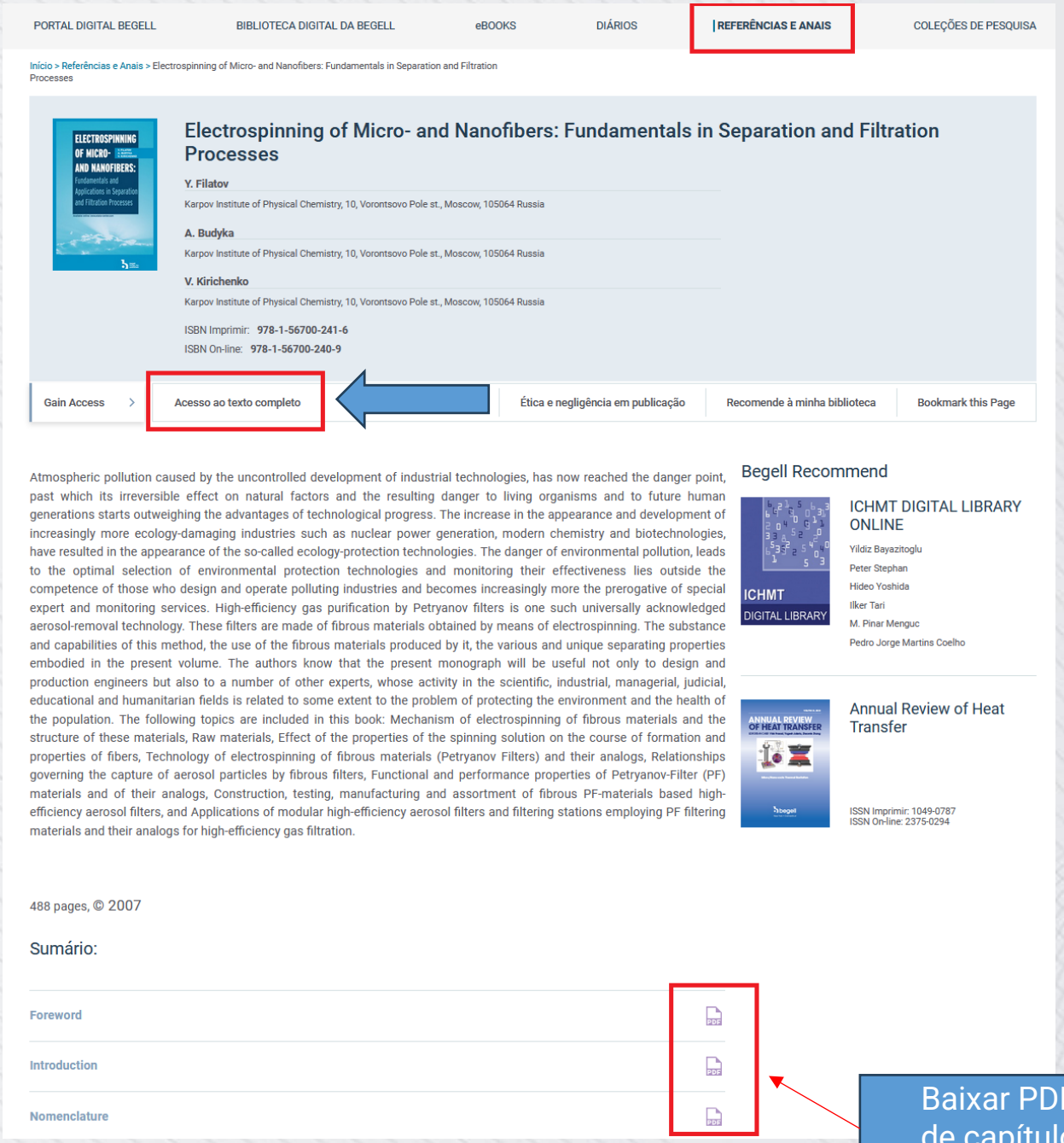

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-
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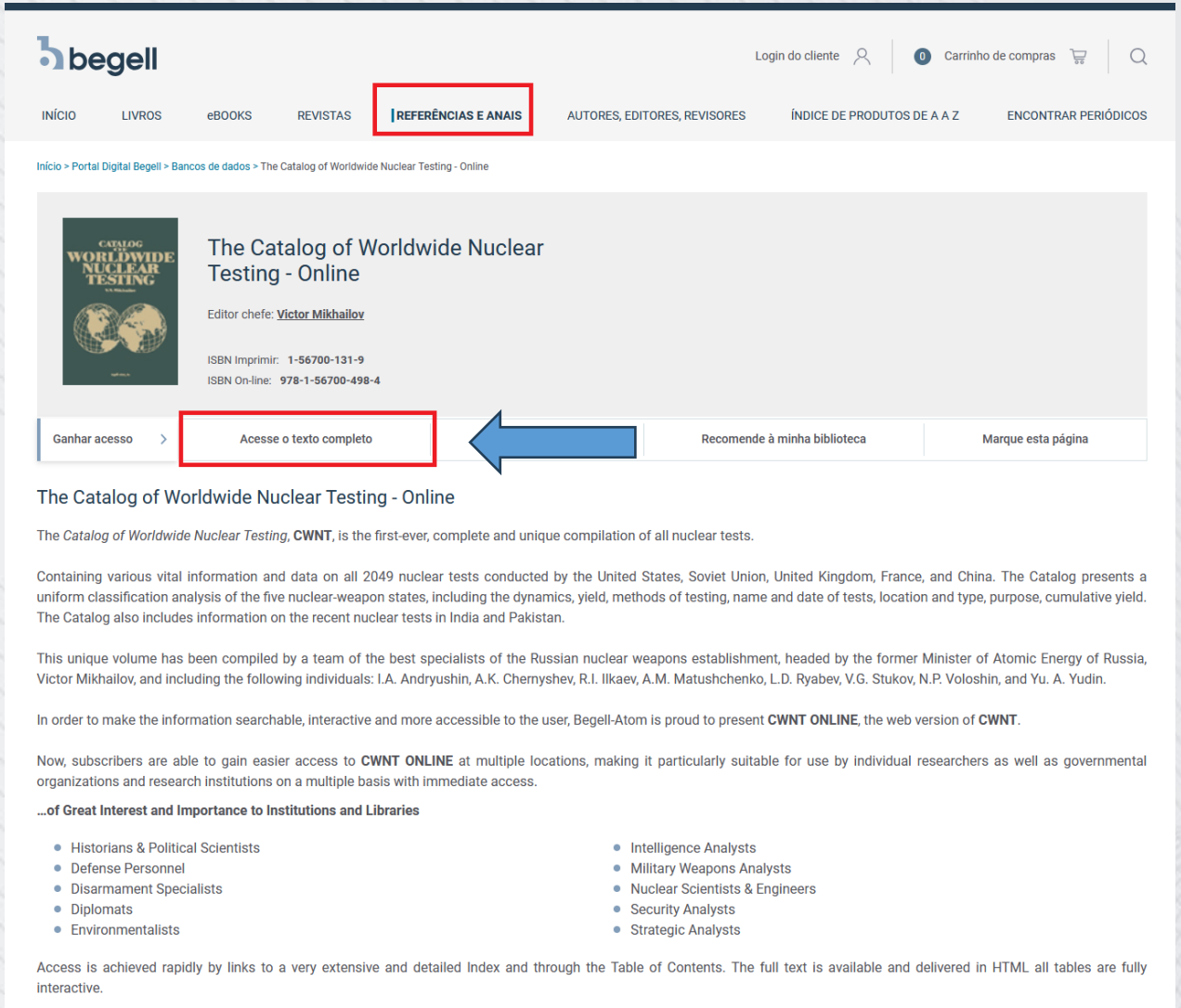

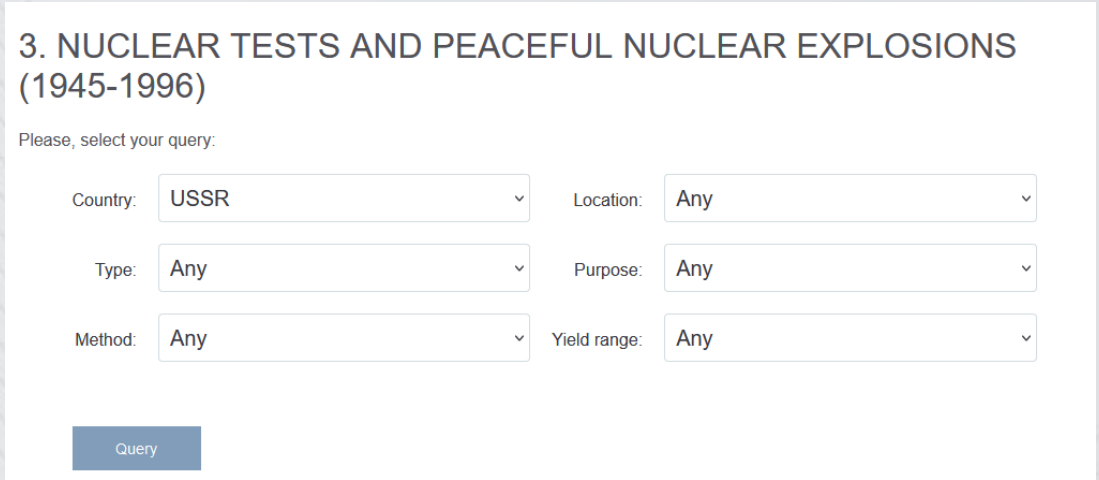

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